

EUROPEAN UNION European Structural and Investment Funds Operational Programme Research, Development and Education





THE EFFECT OF MOISTURE ON SPECIFIC ENERGY DEMAND FOR KNIFE-MILLED WHEAT STRAW

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Mechanical size reduction = INITIAL STEP of waste treatment technologies.

> WHY TO DO IT?

- + An increase of specific surface, bulk density.
- + Increasing efficiency of subsequent treatment.
- + Shearing or defibering of biomass particles.
- + Reduction in degree of polycrystalinity.
- + Easier handling, reducing transportation cost.

SOME LIMITATIONS?

- High energy-demanded.
- Biomass behaviour.
- Technical limits of commercial size reduction machines.

TECHNOLOGY	TARGETED PARTICLE SIZE
Pelleting briquetting	< 6 mm
Pulverized combustion	< 1 mm
Pyrolysis	0.25-2.00 mm
Fluid bed gasification	0.12-10.00 mm
Fermentation	0.03-10 mm
Lignocellulosic distillery	0.5-3.0 mm

MECHANICAL ENERGY NEED TO REDUCE PARTICLES FROM NATIVE/INITIAL TO A TARGETED PARTICLE SIZE BETWEEN MILL WORKING TOOLS

Hendriks A.T.W.M., Zeeman G., 2009, Pretreatment to enhance the digestibility of lignocellulosic biomass, Bioresource Technology, 100, 10-18.
Hoque M., Sokhansanj S., Naimi L., Bi X., Lim J., 2007, Review and analysis of performance and productivity of size reduction equipment for fibrous materials. ASABE Annual International Meeting, Minneapolis, Minnesota.
Oyedeji O., Gitman P., Qu J., Webb E., 2020, Understanding the impact of lignocellulosic biomass variability on the size reduction process: A review, Webb, ACS Sustainable Chemistry and Engineering, 8, 2327-2343.
Miao Z., Grift T.E., Hansen A.C., Ting K.C., 2011, Energy requirement for comminution of biomass in relation to particle physical properties, Industrial Crops and Products, 33, 504-513.



DEFINING AIMS AND NOVELTY

- Specific energy requirement listed as single values.
- A little information served regarding modelling of energy demand on biomass characteristics.
 - regression curves power, exponential, polynomic or linear functions

de

dD

 $\mathbf{C} \cdot D^{-r}$

o conventional models - Bond, Rittinger, or Kick comminution laws

AIMS:

To experimentally identify the effect of biomass characteristics
(flowrate, moisture, initial particle size) and knife mill variables (peripheral speed of the rotor, screen size) on specific energy requirement.
To define and calibrate a model that allows predicting specific energy requirement for knife milling of wheat straw at different moistures.



MATERIAL AND MACHINE

- Wheat straw with moistures 3.1 wt %, 8.1 wt %, 22.9 wt %
- the laboratory knife mill SM300 equipped with a three linear-bladed rotor
 - $_{\odot}$ rotor speeds of 10.2 m s $^{\text{-1}}$ (1500 rpm) and 20.4 m s $^{\text{-1}}$ (3000 rpm)
 - $_{\odot}$ screen sieves of openings 10 6 4 2 -1 0.75 mm





EXPERIMENTAL LAYOUT

Each experimental run characterized by particle size characteristic before/after milling and by specific energy demand.

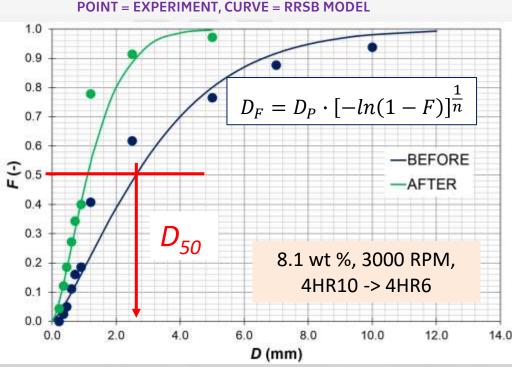
Particle size characteristics:

- Screen sieve analysis by the ASABE standard S424.1.
- Applying RRSB model.
- Identifying D₅₀ value.

Specific energy demand:

 Analysing active power during milling and iddle state by power analyser in period 1 s.

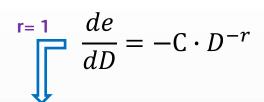
$$e = \frac{1}{m} \cdot \left(\int_{0}^{t} P_{AM} dt - \int_{0}^{t} P_{AI} dt \right)$$





KICK THEORY:

➤ energy need to ensure a particle's elastic

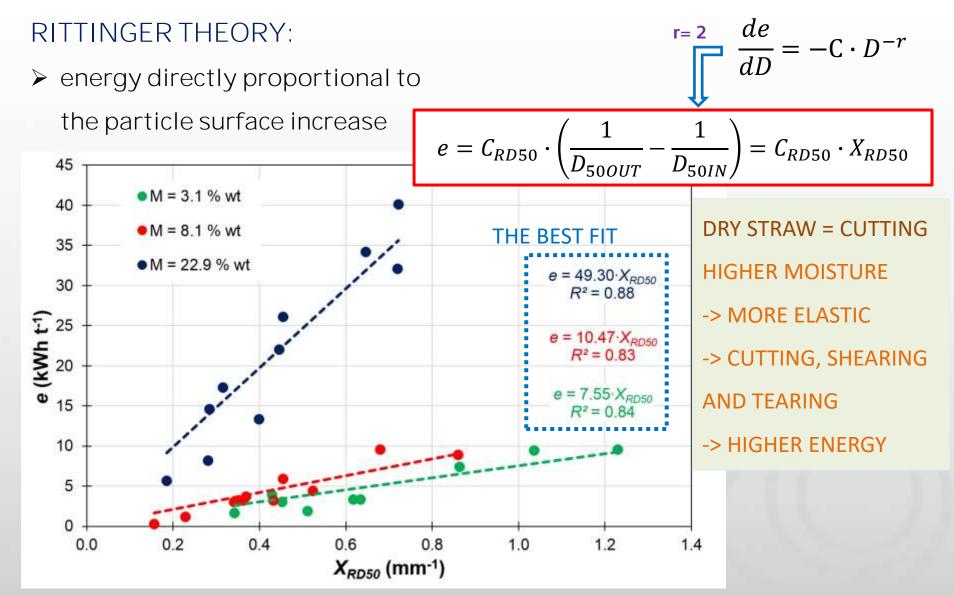


deformation followed by its crack $e = C_{KD50} \cdot ln \frac{1}{D_{500UT}}$ $\frac{D_{50IN}}{D_{50IN}} = C_{KD50} \cdot X_{KD50}$ 45 M = 3.1 % wt 40 • M = 8.1 % wt **JNITS OR LOW DECIMALS** 35 POOR $e = 49.78 \cdot X_{KD50}$ • M= 22.9 % wt $R^2 = 0.10$ PRECISION 30 **HIGHER MOISTURE -> MORE** 1 25 **ELASTIC -> HIGHER** e = 9.54 XKD50 **COMPRESION-> HIGHER** $R^2 = -0.03$ **ENERGY** Φ NOT 15 e = 9.43 XKD50 $R^2 = 0.02$ **APPLICABLE** 10 5 0 0.4 0.6 0.2 0.8 1.0 0.0 X_{KD50} (-)

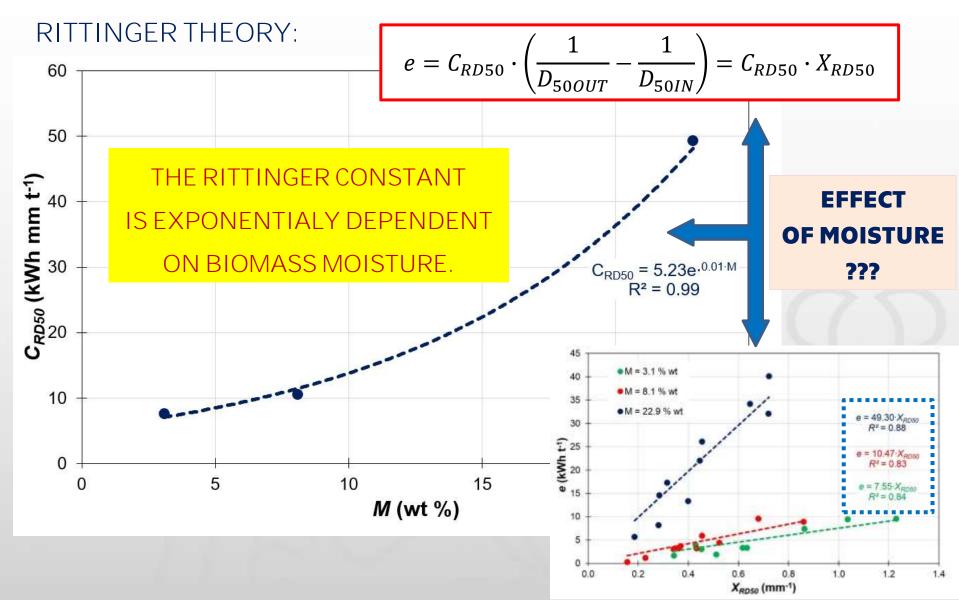


de **BOND THEORY:** r= 1.5 $-\mathbf{C} \cdot D^{-r}$ dDenergy needed for crack propagation is proportional to the new crack length $e=2\cdot C_{BD50}$ $= C_{BD50} \cdot X_{BD50}$ 45 $\sqrt{D_{500UT}}$ $\sqrt{D_{50IN}}$ • M = 3.1 % wt 40 DRY STRAW = CUTTING • M = 8.1 % wt 35 • M = 22.9 % wt HIGHER MOISTURE $e = 54.23 \cdot X_{BD50}$ 30 $R^2 = 0.74$ -> MORE ELASTIC e (kWh t-1) 20 e = 10.99 X BD50 -> CUTTING, SHEARING $R^2 = 0.55$ AND TEARING e = 9.29 X 8050 15 $R^2 = 0.61$ -> HIGHER ENERGY 10 GOOD 5 PRECISION 0 **APPLICABLE** 0.0 0.8 1.0 1.2 0.2 0.4 0.6 X_{BD50} (mm^{-0.5}) ???



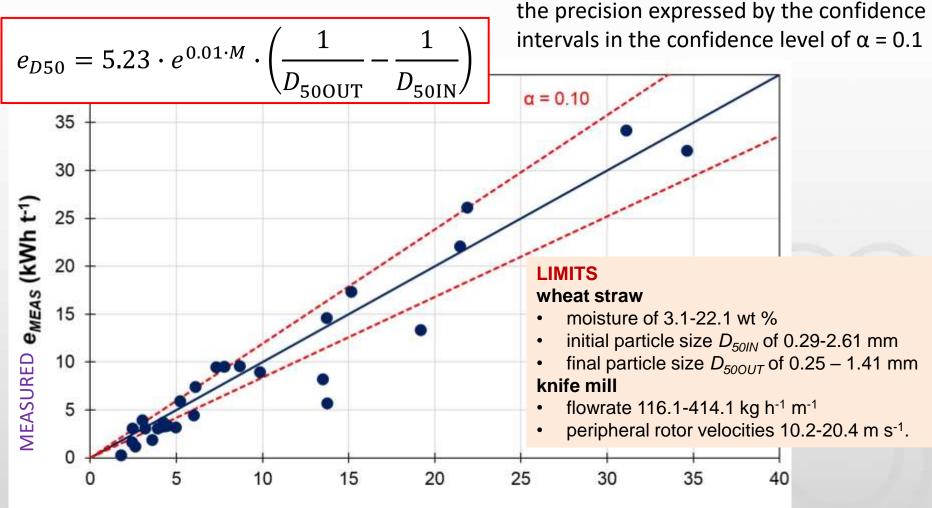








DEFINING PREDICTION MODEL:



CALCULATED BY MODEL *e_{D50CALC}* (kWh t⁻¹)



CONLUSIONS

- The effect of moisture on specific energy demand for knife milled wheat straw experimentally quantified
- The specific energy requirement ranges in units or lower tents of kWh t⁻¹.
- Comminution laws were tested to define mutual relations among specific • energy demand, particle size characteristics and biomass moisture.

MESSAGE TO TAKE HOME:

- The Rittinger comminution law showed the highest precision.
- The value of the Rittinger constant was power law dependent on moisture content. LIMITS

$$e_{D50} = 5.23 \cdot e^{0.01 \cdot M} \cdot \left(\frac{1}{D_{500\text{UT}}} - \frac{1}{D_{50\text{IN}}}\right)$$

wheat straw

- moisture of 3.1-22.1 wt %
- initial particle size $D_{50IN} = 0.29-2.61$ mm
- final particle size $D_{500UT} = 0.25 1.41$ mm knife mill
- flowrate 116.1-414.1 kg h⁻¹ m⁻¹
- peripheral rotor velocities 10.2-20.4 m s⁻¹.



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RESEARCH CENTRE OF LOW-CARBON ENERGY TECHNOLOGIES

CZECH TECHNICAL UNIVERSITY IN PRAGUE FACULTY OF MECHANICAL ENGINEERING Project reg. Nr. CZ.02.1.01/0.0/0.0/16_019/0000753

The presentation and workshop were supported by the International Visegrad Fund under grant number 22120032 named "Green Deal strategies for V4 countries: The need and challenges to reach low-carbon industry".







